

Amendments to the Claims: This listing of claims will replace all prior versions, and listings, of claims in the application

Listing of Claims:

1. (Currently Amended) A vacuum distillation plant, comprising:
 - a) a flash evaporator for producing an overhead product and a bottoms product;
 - b) vapor concentration means downstream of said flash evaporator to receive said overhead product;
 - c) a multi-stage ~~condenser~~ heat exchanger downstream of said vapor concentration means to separate a more volatile portion of said overhead product from a less volatile component of said overhead product;
 - d) rectification means between said ~~condenser~~ heat exchanger stages;
 - e) means for recycling at least part of a condensate from a ~~condensation~~ second heat exchanger stage to said bottoms product of said flash evaporator, said bottoms product of said flash evaporator is passed through said ~~condenser~~ heat exchanger stages to serve as a heat carrier liquid for the ~~condenser~~ heat exchanger before being recycled to the evaporator, whereby a user can use said means for recycling to maintain a ratio of more volatile to less volatile constituents in a solution undergoing concentration in said distillation plant.
2. (Canceled)
3. (Canceled)
4. (Currently Amended) A vacuum distillation plant according to claim 1 wherein two to four ~~condensation~~ stages are provided in said heat exchanger with a rectification interposed between each of said condensation stages.
5. (Currently Amended) A vacuum distillation plant according to claim 1, wherein all or part of the condensate of the last ~~condensation~~ heat exchanger stage is recycled to the evaporator.
6. (Currently Amended) A vacuum distillation plant according to claim 5 comprising two ~~condensation~~ heat exchanger stages.

7. (Previously Presented) A vacuum distillation plant according to claim 1 wherein the condensate is recycled into the evaporator above the liquid level of the bottoms product.

8. (Previously Presented) A vacuum distillation plant according to claim 1 wherein the condensate is introduced into and mixed with the bottoms product and the mixture is introduced into the evaporator.

9. (Currently Amended) A vacuum distillation plant according to claim 1, additionally comprising means for actively directing the bottoms product through the ~~condenser~~heat exchanger stages.

10. (Original) A vacuum distillation plant according to claim 9 wherein the means for actively directing the bottoms product is a circulating pump.

11. (Previously Presented) A vacuum distillation plant according to claim 1 comprising a pre-vacuum pump in addition to the concentration means.

12. (Original) A vacuum distillation plant according to claim 11, wherein the pre-vacuum pump is an oil-driven liquid-ring pump.

13. (Currently Amended) A vacuum distillation plant according to claim 1, comprising means on the condensate side for depositing solid and/or liquid components entrained in the overhead product from said ~~fluid~~-evaporation during flash evaporation.

14. (Currently Amended) A process for concentration of aqueous alcoholic solutions wherein:

a) ~~expanding said solution is under~~using a vacuum distillation to form an overhead product and a bottoms product being a concentrated aqueous alcoholic solution;

b) pressurizing and transporting said overhead product to a multi-stage ~~condenser~~heat exchanger;

c) separating said overhead product into its less volatile and more volatile components in a~~said~~ multi-stage ~~condenser~~heat exchanger; and

d) using at least part of the condensate from at least one stage of said ~~condenser~~heat exchanger to form a bottoms product having a desired concentration for recycle to step a) wherein the bottoms product is used as a heat carrier liquid for the ~~condensation-heat exchanger~~stages.

15. (Canceled)

16. (Previously Presented) A process according to claim 14, wherein two condensation steps are carried out in step c) starting from binary solutions and wherein at least part of the condensate of the second step is recycled to the bottoms product.

17. (Previously Presented) A process according to claim 14, wherein the condensate is recycled in an amount so that the water to alcohol ratio of the solution in the bottoms product remains constant.

18. (Canceled)

19. (Previously Presented) A process according to claim 14 including the steps of concentrating aqueous ethanolic plant drug extracts having an ethanol content of at least 20 vol.-%.

20. (Canceled)

21. (Canceled)

22. (Cancelled)

23. (Canceled)

24. (Canceled)

25. (Canceled)

26. (Canceled)

27. (Currently Amended) A vacuum distillation plant according to claim 4, wherein all or part of the condensate of the last ~~condensation~~ heat exchanger stage is recycled to the evaporator.

28. (Canceled)

29. (Canceled)

30. (Previously Presented) A vacuum distillation plant according to claim 4, wherein the condensate is recycled to the flash evaporator above the liquid level of the bottoms product.

31. (Previously Presented) A vacuum distillation plant according to claim 5, wherein the condensate is fed into the evaporator above the liquid level of the bottoms product.

32. (Previously Presented) A vacuum distillation plant according to claim 6, wherein the condensate is recycled into the evaporator above the liquid level of the bottoms product.

33. (Canceled)

34. (Canceled)

35. (Previously Presented) A vacuum distillation plant according to claim 4, wherein the condensate is introduced into and mixed with the bottoms product and the mixture is introduced into the evaporator.

36. (Previously Presented) A vacuum distillation plant according to claim 5, wherein the condensate is introduced into and mixed with the bottoms product and the mixture is introduced into the evaporator.

37. (Previously Presented) A vacuum distillation plant according to claim 6, wherein the condensate is introduced into and mixed with the bottoms product and the mixture is introduced into the evaporator.

38. (Previously Presented) A vacuum distillation according to claim 7, wherein the condensate is introduced into and mixed with the bottoms product and the mixture is introduced into the evaporator.

39. (Currently Amended) A process according to claim 14, wherein two ~~condensation~~ heat exchanger steps are carried out in step c) starting from binary solutions and wherein at least part of the condensate of the second heat exchanger step ~~stage~~ is recycled to the bottoms product.

40. (Previously Presented) A process according to claim 14, wherein the condensate is recycled in such an amount that the water/alcohol ratio of the solution in the bottoms product remains constant.

41. (Previously Presented) A process according to claim 16, wherein the condensate is recycled in such an amount that the water to alcohol ratio of the solution in the bottoms product remains constant.

42. (Canceled)

43. (Previously Presented) A process according to claim 16, wherein the bottoms product is distilled by flash evaporation.

44. (Previously Presented) A process according to claim 17, wherein the bottoms product is distilled by flash evaporation.

45. (Previously Presented) A process according to claim 14, including the steps of concentrating aqueous ethanolic plant drug extracts having an ethanol content of at least 20 vol.-%.

46. (Previously Presented) A process according to claim 16, including the steps of concentrating aqueous ethanolic plant drug extracts having an ethanol content of at least 20 vol.-%.

47. (Previously Presented) A process according to claim 17, including the steps of concentrating aqueous ethanolic plant drug extracts having an ethanol content of at least 20 vol.-%.

48. (Previously Presented) A process according to claim 18, including the steps of concentrating aqueous ethanolic plant drug extracts having an ethanol content of at least 20 vol.-%.

49. (Previously Presented) A process according to claim 14, including the step of concentrating aqueous ethanolic plant drug extracts having an ethanol content of from 30 to 70 vol.-%.

50. (Currently Amended) A process for concentrating a plant extract in form of an aqueous alcoholic solution wherein:

a) ~~the solution is expanded under~~ using vacuum distillation to form an overhead product and a bottoms product being a concentrated plant extract;

b) pressurizing and transporting said overhead product to a multi-stage ~~condenser~~ heat exchanger;

c) separating said overhead product into its less volatile and more volatile components; and

d) using at least part of the condensate from at least one stage of said ~~condenser~~ heat exchanger to form a bottoms product having a desired concentration for recycle to step a).

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51. (Canceled)